

CHAETOMORPHA LINUM EXTRACT AS A GREEN INHIBITOR FOR CORROSION OF BRASS IN 0.1 N PHOSPHORIC ACID SOLUTION

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ABSTRACT

The effect of marine algae *Chaetomorpha linum* extract on corrosion inhibition of brass in phosphoric acid was investigated by weight-loss method, potentiodynamic polarization and electrochemical impedance spectroscopy studies. The inhibition efficiency is found to increase with increasing concentration of extract and decreases with rise in temperature. The inhibitive effect could be attributed to the phytochemical constituents present in the inhibitor containing N, S, O atoms. The activation energy, thermodynamic parameters (free energy, enthalpy and entropy change) and kinetic parameters (rate constant and half-life) for inhibition process were calculated. These thermodynamic and kinetic parameters indicate a strong interaction between the inhibitor and the brass surface. The inhibition is assumed to occur via adsorption of inhibitor molecules on the brass surface, which obeys Temkin adsorption isotherm. The adsorption of inhibitor on the brass surface is exothermic, physical, and spontaneous, follows first order kinetics. The polarization measurements showed that the inhibitor behaves as a mixed type inhibitor and the higher inhibition surface coverage on the brass was predicted. Inhibition efficiency values were found to show good trend with weight-loss method, potentiodynamic polarization and electrochemical impedance spectroscopy studies. Surface analytical techniques (FT-IR and SEM) were carried out to ascertain the inhibitive nature of the algal extract on the brass surface.

Index Terms: Brass, Phosphoric acid, *Chaetomorpha linum*, Inhibition, Polarization, and Isotherm.

1. INTRODUCTION

Phosphoric acid (H_3PO_4) is a major chemical product, which has many important uses especially in the production of fertilizers. Most of the acid is produced from phosphate rock by wet process. Brass and stainless steel are frequently used in many parts of the wet process and a considerable quantity of data has been published about the resistance of these materials to corrosion by acid solutions [1,2]. Most of the previous studies were focused on the inhibition of metals in HCl or H_3PO_4 solutions using organic compounds containing N, S, O atoms as corrosion inhibitors [3-5]. A lot of research has been done with naturally occurring substances since they are known to be eco-friendly and with little or no side effect on the humans. Among the naturally occurring substances reported in the corrosion study of metals like brass, aluminium, tin and mild steel, there leave extracts, gums and exudates, dyes, oils from plant materials, plant seeds and fruits, and anti-bacterial drugs. Plant extracts like the extract of *Cocos nucifera*-coconut palm-petiole [6]; *Musa Paradisiaca* [7]; *Mentha Pulegium* [8]; *Treulia Africana* leaves [9] and *Lupinus varius* leaves [10] have been studied and established their corrosion inhibition effects. They were all found to be good corrosion inhibitors with no effect on the environment.

In the present study, the effect of addition of marine algae *Chaetomorpha linum* extract on corrosion inhibition of

brass in 0.1 N phosphoric acid solutions at different temperatures and various time intervals have been investigated by weight-loss method, potentiodynamic polarization and electrochemical impedance spectroscopy studies. The weight loss measurements aimed to predict the inhibition efficiency on brass corrosion and the adsorption isotherm, thermodynamic and kinetic feasibility of inhibition via surface coverage on brass by adsorbed *Chaetomorpha linum* extract. The inhibition type and inhibition efficiency were determined from the polarization measurements and impedance spectroscopy studies. Surface analytical techniques (FT-IR and SEM) were carried out to ascertain the inhibitive nature of the algal extract on the brass surface.

2. MATERIAL AND METHODS

2.1 MATERIALS

The chemical composition (weight percent) of the brass used in the present study was 71.5 % Cu, 28.38 % Zn, 0.07 % Pb, and 0.05 % Fe. The geometry of the specimens for weight-loss experiments was as follows: The brass specimens were polished mechanically with different grades of emery papers (1/0 to 4/0) and were thoroughly washed with double distilled water then degreased in acetone and dried. The solutions were prepared from analar grade chemicals using double distilled water. Phosphoric acid solution (H_3PO_4) was used as a

corrosion medium. The inhibitor *Chaetomorpha linum* extract (CLE) was extracted with ethanol using soxhelt extractor from marine algae *Chaetomorpha linum*.

2.2 WEIGH-LOSS MEASUREMENT

Measurements of weight changes were performed with rectangular brass specimens (length: 5 cm, width: 1 cm, and thickness: 0.3 cm). The specimens with same dimensions were immersed in 100 ml of 0.1 N H₃PO₄ solutions with and without different concentrations (0.0001 % to 0.0005 %) of CLE and allowed stand for 3 h and 6 h at various temperatures were as follows: 300 K, 318 K, 328 K, and 338 K. At 300 K the specimens were immersed for immersion time of 24, 48, 72, and 96 h. Then, the specimens were rinsed with distilled water and adherent corrosion products for 20 s. then the specimens were rinsed with water, cleaned with acetone and dried. The percentage of inhibition efficiency (IE) over the exposure period was calculated using the following equation (1) [11]:

$$\text{Inhibition efficiency (\%)} = \frac{W_o - W_i}{W_o} \times 100 \quad (1)$$

where W_o and W_i are the rate of corrosion for brass with and without inhibitor, respectively.

2.3 POTENTIODYNAMIC POLARIZATION STUDIES

The potentiodynamic polarization studies were carried out with brass strips having an exposed area of 1 cm². The cell assembly consisted of brass as working electrode, a platinum foil as counter electrode and a saturated calomel electrode as a reference electrode. Polarization studies were carried out using a potentiostat/galvanostat (Model BAS-100 A). The working electrode was immersed in a 0.1 N H₃PO₄ and allowed to stabilize for 30 min. Each electrode was immersed in a 0.1 N H₃PO₄ in the presence and absence of different concentrations of inhibitor to which a current of 1.5 mA/cm² was applied for 20 minutes to reduce oxides. The cathodic and anodic polarization curves for brass specimen in the test solution with and without various concentrations of the inhibitor were recorded by scanning the potential range ± 200 from the corrosion potential at a sweep rate of 1 mV/s. The inhibition efficiencies were determined from corrosion currents using the Tafel extrapolation method. The corrosion inhibition efficiency (IE) was calculated from the following equation (2):

$$\text{IE (\%)} = \frac{i_{\text{corr}} - i_{\text{corr}(i)}}{i_{\text{corr}}} \times 100 \quad (2)$$

Where i_{corr} and $i_{\text{corr}(i)}$ are the corrosion current density values without and with inhibitor, respectively.

2.4 ELECTROCHEMICAL IMPEDANCE SPECTROSCOPY STUDIES

A well polished brass electrode was introduced into 100 ml of test solution and allowed to attain a steady potential value. AC signal of amplitude of 10mV was applied and the frequency was varied from 10 MHz to 10 KHz using Solartron electrochemical measurement unit (1280B). The real and imaginary parts of the impedance were plotted in Nyquist plots as shown in Figure 5. From the Nyquist plot, the charge transfer resistance (R_{ct}) and double layer capacitance (C_{dl}) values were calculated.

The charge transfer resistance values were obtained from the plots of Z' vs Z'' . The values of ($R_s + R_{ct}$) correspond to the point where the plots cuts Z' axis at low frequency and R_s corresponds to the point where the plot cuts Z' axis at high frequency. The difference between R_{ct} and R_s values give the charge transfer resistance (R_{ct}) values. The C_{dl} values were obtained from the following equation (3):

$$C_{dl} = \frac{1}{2\pi f_{\text{max}} \times R_{ct}} \quad (3)$$

where C_{dl} is double layer capacitance, R_{ct} is charge transfer resistance and f_{max} is frequency at Z'' value maximum.

The inhibition efficiencies were calculated from R_{ct} values using the following equation (4):

$$\text{IE\%} = \frac{R_{ct(i)} - R_{ct}}{R_{ct(i)}} \times 100 \quad (4)$$

where R_{ct} and $R_{ct(i)}$ are the charge transfer resistance in the absence and presence of inhibitor respectively.

2.5 SURFACE STUDY

The brass specimen was immersed in 0.1 N H₃PO₄ in the presence of inhibitor for 6 h at 300 K. After 6 h the specimen was taken out and dried. The nature of the film formed on the brass surface was analyzed by FT-IR Perkin Elmer-1600 spectrometer. SEM images were recorded with a Hitachi 3000 H Microscope from the dried film formed on the surface of the brass specimens taken from 0.1 N H₃PO₄ in the presence and absence of inhibitor immersed for 6 h at 300 K.

3. RESULTS AND DISCUSSION

3.1 WEIGH-LOSS METHOD

Table-1 shows the inhibition efficiency values of brass by weight-loss measurements at different inhibitor concentrations in 0.1 N H₃PO₄ for different immersion times and temperatures. It has been observed that the inhibition efficiency increases with increase in concentration of inhibitor and decreases with increase in temperature and immersion time. The maximum IE (78.95 %) of inhibitor was achieved at 0.0005 % of inhibitor at 300 K for 3 h.

Table -1: Calculated inhibition efficiency (IE) and surface coverage (SC) values for CLE on brass corrosion in 0.1 N H₃PO₄ for different immersion temperatures and times

Conc. of inhibitor (%)	For 3 h		For 6 h		At 300 K	
	SC (θ)	IE (%)	SC (θ)	IE (%)	SC (θ)	IE (%)
	300 K				24 h	
0.0000	0	0	0	0	0	0
0.0001	0.4211	42.11	0.2692	26.92	0.2857	28.57
0.0002	0.4737	47.37	0.3462	34.62	0.3117	31.17
0.0003	0.6316	63.16	0.3846	38.46	0.3507	35.07
0.0004	0.6842	68.42	0.5000	50.00	0.4026	40.26
0.0005	0.7895	78.95	0.6539	65.39	0.4675	46.75
	318 K				48 h	
Blank	0	0	0	0	0	0
0.0001	0.3333	33.33	0.2121	21.21	0.2191	21.91
0.0002	0.4286	42.86	0.3030	30.30	0.2303	23.03
0.0003	0.5238	52.38	0.3636	36.36	0.2528	25.28
0.0004	0.5714	57.14	0.4546	45.46	0.3034	30.34
0.0005	0.6667	66.67	0.6061	60.61	0.3820	38.20
	328 K				72 h	
Blank	0	0	0	0	0	0
0.0001	0.2500	25.00	0.1786	17.86	0.1857	18.57
0.0002	0.3750	37.50	0.2321	23.21	0.2236	22.36
0.0003	0.4167	41.67	0.2679	26.79	0.2405	24.05
0.0004	0.5000	50.00	0.3036	30.36	0.2700	27.00
0.0005	0.5833	58.33	0.4107	41.07	0.3291	32.91
	338 K				96 h	
Blank	0	0	0	0	0	0
0.0001	0.1765	17.65	0.1642	16.42	0.1398	13.98
0.0002	0.2647	26.47	0.1791	17.91	0.1550	15.50
0.0003	0.3823	38.23	0.2239	22.39	0.1672	16.72
0.0004	0.4706	47.06	0.2836	28.36	0.2006	20.06
0.0005	0.5882	58.82	0.3881	38.81	0.2584	25.84

3.2 THERMODYNAMIC AND KINETIC ANALYSIS

The adsorption of the organic compounds can be described by two main types of interactions: physical adsorption and chemisorptions. They are influenced by the nature of the charge of the metal, the chemical structure of the inhibitor, pH, the type of the electrolyte and temperature [6].

3.2.1 ACTIVATION ENERGY

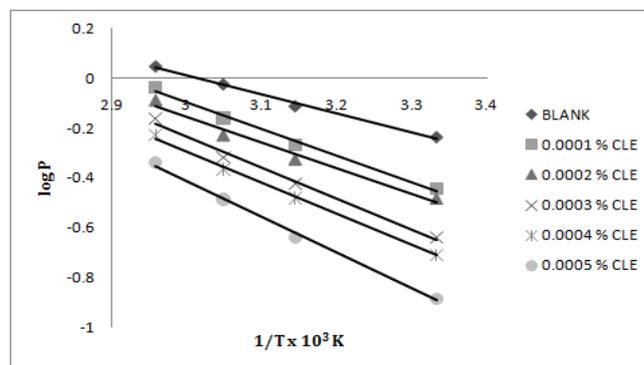
In order to elucidate the inhibitive properties of the inhibitor and the temperature dependence on the corrosion rates, the energy of activation for the corrosion process in the absence and presence of the inhibitor was evaluated from the following Arrhenius equation (4) and the values obtained are presented in Table-2:

$$\log \frac{p_2}{p_1} = \frac{E_a}{2.303 \times R} \left[\frac{1}{T_1} - \frac{1}{T_2} \right] \quad (5)$$

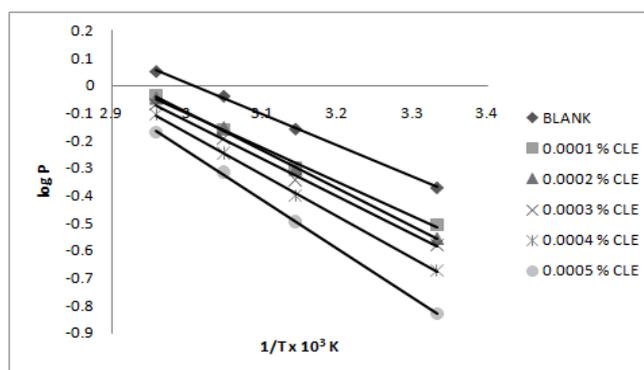
where p_1 and p_2 are rate of corrosion at temperatures T_1 and T_2 respectively.

Arrhenius plot for the corrosion rate of brass in the presence CLE for 3 h and 6 h are given in Figure 1: (a)-(b). Straight lines were obtained from the plot of Log P versus $1/T$ with slope equal to $-E_a / 2.303 R$. Note first that the E_a values are low, indicating fast corrosion of brass in both the solutions [13]. The values of E_a calculated from the slopes of Arrhenius plot and by using equation (4) are approximately almost similar.

The estimated values of E_a for brass corrosion in the presence of CLE are listed in the Table -2. The values of $E_a > 80$ KJ/mol indicate chemical adsorption where as $E_a < 80$ KJ/mol infer physical adsorption. The E_a values indicate that the process is activation controlled. In the present study, the E_a values support the fact that the inhibitors are physically adsorbed on brass surface. The estimated E_a in the presence of inhibitor infer that the interaction between the metal surface and the inhibitor was found to be strong enough to reduce corrosion [13]. The E_a values increases in the presence of CLE is often interpreted as physical adsorption with the formation of an adsorptive film with an electrostatic character [12]. In addition, the E_a values increases in the same order as the inhibition efficiency. This indicates that the energy barrier for the corrosion reaction increases in the presence of inhibitor in the acid solutions, the corrosion reaction will be further pushed to surface sites that are characterized by higher values of E_a indicating that corrosion occurs at the uncovered part of the surface [15].



(a)



(b)

Figure 1: Arrhenius plot for 0.1 N H_3PO_4 with different concentrations of CLE for different times

3.2.2 FREE ENERGY OF ADSORPTION

The free energy of adsorption ΔG_{ads} were obtained from the following equations and the values obtained are presented in Table-2:

$$\Delta G_{ads} = -RT \ln (55.5K) \quad (6)$$

where K is given by

$$K = \frac{\theta}{C(1-\theta)} \quad (7)$$

where θ is surface coverage on the metal surface, C is the concentration of inhibitor in mol/l and K is equilibrium constant.

Results obtained indicate that the values of ΔG_{ads} are negative in all cases, indicating that the CLE extract is strongly adsorbed on the brass surface [14]. The value of ΔG_{ads} indicates that the inhibitor functions by physically adsorbing on the surface of the brass. Generally values of ΔG_{ads} upto the -29.47 KJmol⁻¹ are consistent with electrostatic interaction between charged molecules and a charged metal, while those more negative than the -40 KJmol⁻¹ involve charge sharing or transfer from the inhibitor molecules to the metal surface to form a co-ordinate type of bond [15]. Physical adsorption is a result of electrostatic attraction between charged metal surface and charged species in the bulk of the solution. Adsorption of negatively charged species can also protect the positively charged metal surface acting with a

negatively charged intermediate such as acid anions adsorbed on the metal surface [6].

Table -2: Calculated activation energy (E_a), free energy of adsorption (ΔG_{ads}), enthalpy change (ΔH), entropy change (ΔS) values for CLE on brass corrosion in 0.1 N H_3PO_4 at 300 K

Conc. of inhibitor (%)	E_a from equation (kJ/mol)	E_a from Arrhenius Plot (kJ/mol)	ΔG_{ads} (kJ/mol)	ΔH (kJ/mol)	ΔS (mol/kJ)
For 3 Hours					
Blank	12.91	12.98	0	0	0
0.0001	20.73	19.15	-29.47	-24.75	0.0157
0.0002	20.33	21.28	-27.80	-24.73	0.0102
0.0003	24.37	22.68	-26.61	-24.72	0.0063
0.0004	24.38	23.94	-25.71	-24.70	0.0034
0.0005	27.79	27.36	-24.50	-24.67	0.0006
For 6 Hours					
Blank	21.00	16.76	0	0	0
0.0001	23.99	23.94	-28.94	-24.70	0.0141
0.0002	26.05	25.53	-27.56	-24.69	0.0096
0.0003	26.15	29.93	-26.66	-24.64	0.0067
0.0004	28.98	28.16	-26.08	-24.66	0.0047
0.0005	33.65	31.92	-25.27	-24.62	0.0022

3.2.3 ENTROPY AND ENTHALPY

Kinetic parameters such as enthalpy (ΔH) and entropy (ΔS) of activation of corrosion process is calculated from the following thermodynamic basic equations and the values obtained are presented in Table-2:

$$\Delta H = E_a - RT \quad (8)$$

$$\Delta G_{ads} = \Delta H - T\Delta S \quad (9)$$

Enthalpy of activation of absolute values lower than the -24.75 $KJmol^{-1}$ indicates physical adsorption, and the values approaching 100 $KJmol^{-1}$ indicate chemical adsorption. In this study, the values of ΔH are lower than the -24.75 $KJmol^{-1}$ confirming physical adsorption on the acid solutions [10]. The negative values of ΔH also show that the adsorption of inhibitor is an exothermic process [14].

The ΔS values are positive for the acidic bath. This implies that the activation complex is the rate determining step representing association rather than dissociation, indicating that a decrease in disorder takes place on going from reactant to the activated complex [10].

3.2.4 RATE CONSTANT AND HALF LIFE

Figure 2: show the plots of $\log W_f$ (final weight loss) obtained in weight-loss studies vs. time in days for the brass dissolution. From the plots, the values of rate constant and half-life were evaluated using the following equations [16,17] and the values obtained are presented in Table-3:

$$\text{Rate constant (k)} = 2.303 \times \text{slope (sec}^{-1}) \quad (10)$$

$$\text{Half - life period } t_{1/2} = \frac{0.693}{k} \text{ (sec)} \quad (11)$$

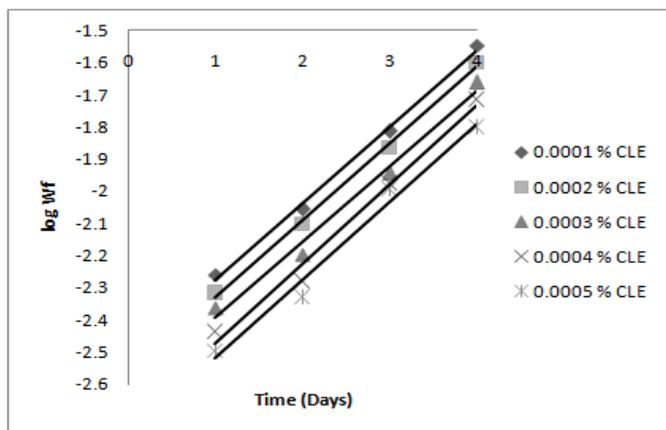


Figure 2: Plot of log W_f vs. time (days) for 0.1 N H_3PO_4 with different concentrations of CLE

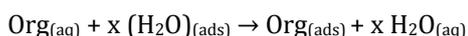
In this study, linear plots were obtained, which indicates first order kinetics [9]. In this study the rate constant values were decreased where as the half-life values were increased with increasing concentration of CLE.

Table -3: Calculated rate constant (k) and half-life period ($t_{1/2}$) values for CLE on brass corrosion in 0.1 N H_3PO_4 at 300 K

Conc. of inhibitor (%)	Rate constant (sec^{-1})	Half-life Period (sec)
0.0001	0.5117	1.3542
0.0002	0.5117	1.3542
0.0003	0.5117	1.3542
0.0004	0.5315	1.3038
0.0005	0.5758	1.2037

3.2.5 ADSORPTION ISOTHERMS

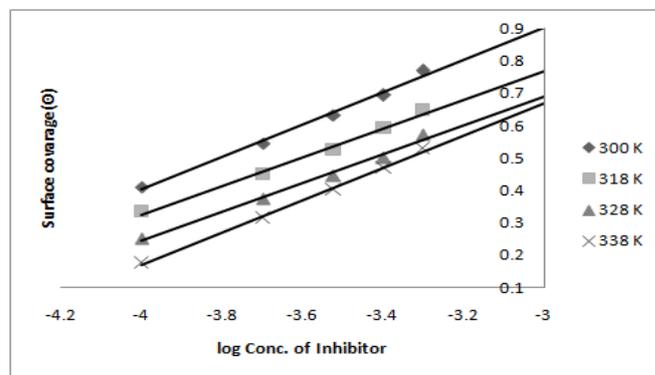
The values of surface coverage θ for different concentrations of the CLE at 300 K have been used to identify the best isotherm to determine the adsorption process. The adsorption of organic adsorbate on the surface of copper is regarded as substitutional process between the organic compound in the aqueous phase org_{aq} and the water molecules adsorbed on the copper surface $(H_2O)_{ads}$ [18].



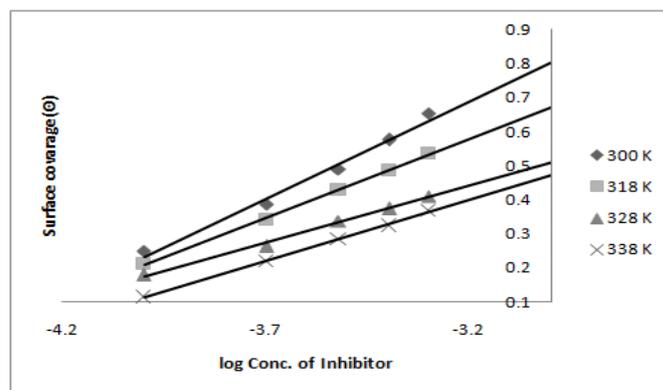
where x is the size ratio, that is the number of water molecules displaced by one molecule of organic inhibitor. Attempts were made to fit θ values of various isotherms, including Langmuir, Freundlich, Temkin and Frumkin isotherms. By far the results were best fitted by Temkin adsorption isotherm. The Temkin adsorption isotherm is given by the following equation.

$$\ln kC = a\theta$$

where k is the equilibrium constant of the adsorption reaction, C is the inhibitor concentration in the bulk of the solution and a is the molecule interaction parameters depending upon molecular interactions in the adsorption layer and the degree of heterogeneity of the metal surface. The plot of θ against $\log C$ for all additives gives straight lines, as shown in Figure 3: (a)-(b). This indicates that these compounds are adsorbed on the surface of brass according to Temkin adsorption isotherm [19,20].



(a)



(b)

Figure 3: Temkin's adsorption isotherm plot for 0.1 N H_3PO_4 with different concentration of CLE for different times

3.3 POTENTIOSTATIC POLARIZATION STUDIES

Polarization measurement is an important research tool in the investigation of a variety of electrochemical phenomena. Such measurements permit studies of the reaction mechanism and the kinetics of corrosion phenomena on the metal deposition. Figure 4: shows the cathodic and anodic polarization curves of brass in 0.1 N H_3PO_4 with and without addition different concentrations of CLE. Table-4 gives the values of associated electrochemical parameters. The i_{corr} values decreased with increasing concentration of inhibitor. The values of anodic Tafel slope (b_a) and cathodic Tafel slope (b_c) of CLE added solutions are found to change with inhibitor concentration, which clearly indicates that the inhibitors controlled both the anodic and cathodic reactions. The IE of CLE attained a maximum value at 0.0005 % concentration of inhibitor. The values of IE increased with increasing concentration of inhibitor, indicating that a higher surface coverage was obtained in solution with optimum concentration of inhibitor. The

effect of the anodic polarization behavior of brass (Figure 4) suggests that protective films formed on the metal surface can alter anodic dissolution in solution shows that

CLE formed a film that acted as a barrier to protect the metal surface [19-21].

Table -4: Electrochemical parameters and inhibition efficiency (IE) for corrosion of brass in 0.1 N H₃PO₄ containing different concentrations of CLE

Conc. of inhibitor (%)	OCP (mV) vs. SCE	E _{corr} (mV) vs. SCE	Tafel constants		i _{corr} (μA/cm ²)	IE (%)
			b _a (mV/dec)	b _c (mV/dec)		
Blank	-193	-190	300	100	310	0
0.0001	-200	-198	300	95	290	6.45
0.0002	-220	-222	280	160	240	22.58
0.0003	-228	-230	160	150	180	41.94
0.0004	-236	-236	90	140	160	48.39
0.0005	-245	-240	50	150	89	71.29

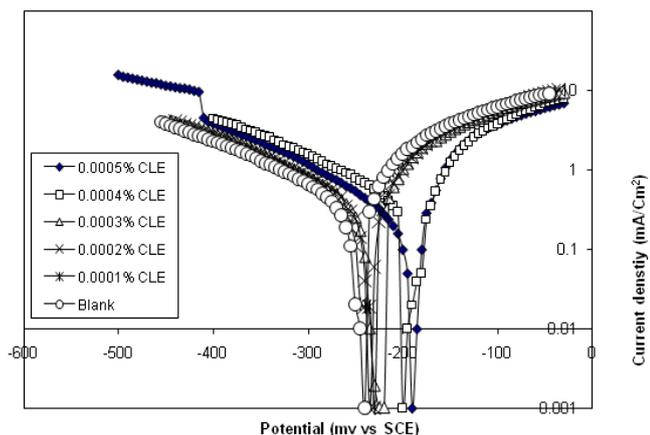


Figure 4: Polarization curves for brass in 0.1 N H₃PO₄ with different concentrations of CLE

3.4 AC IMPEDANCE MEASUREMENTS

AC impedance spectroscopy has been shown to be a powerful tool to study the corrosion process of metals in different environments and to characterize the inhibition ability of a corrosion inhibitor, which is related to the charge transfer resistance (R_{ct}). The double layer capacitance (C_{dl}) can also be used to determine the inhibition ability. The inhibition performance of an organic or natural substance on a metal surface depends not only on the chemical structure of the organic substance and the nature of the metal, but also on the experimental conditions such as the immersion time and concentration of the adsorbent. The corrosion behavior of brass, in acidic solution with and without CLE, is also investigated by AC impedance measurements at 300 K (Figure 5). The impedance parameters and the IE %

derived from the investigation are mentioned given in Table-5. As it can be seen from Figure 5:, impedance diagrams show a semi-circular appearance, indicating that a charge transfer process mainly controls the corrosion of brass. From the impedance data, we notice an increase in the charge transfer resistance and decrease of the double layer capacitance with increasing the inhibitor concentration, indicating that PPE inhibits the corrosion rate of brass by an adsorption mechanism. Therefore, the decrease in the C_{dl} value can be attributed to a decrease in the local dielectric constant and/or an increase in the thickness of the electrical double layer, suggesting that the inhibitor molecules act by adsorption at the metal/solution interface as a consequence of the replacement of water molecules by the inhibitor molecules [8].

A comparison may be made between the inhibition efficiency values obtained by different methods (weight loss, potentiostatic polarization and AC impedance methods). We can see that whatever the method used, no significant changes are observed in IE % values. We can then conclude that there is a good agreement with the three methods used in this study at all tested concentrations and that the acid extract of *Chaetomorpha linum* acts as a green inhibitor for acid corrosion of brass.

Table -5: Impedance measurements and inhibition efficiency (IE) for corrosion of brass in 0.1 N H₃PO₄ containing different concentrations of CLE

Conc. of inhibitor (%)	R _{ct} (ohm cm ²)	C _{dl} (μF/cm ²)	IE (%)
Blank	150.60	5.74	00.00

0.0001	520.18	2.21	71.05
0.0002	685.18	1.80	78.02
0.0003	1300.17	1.01	88.42
0.0004	1910.68	0.73	92.12
0.0005	7370.33	0.19	97.96

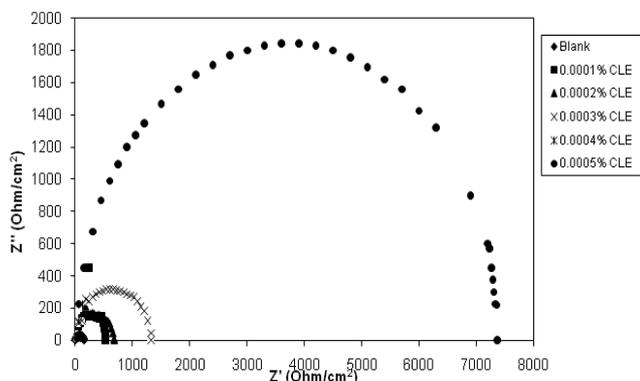


Figure 5: Nyquist plot of brass in 0.1N H₃PO₄ with different concentrations of CLE

3.5 SURFACE EXAMINATIONS

3.5.1 FT-IR SPECTROSCOPY

Figure 6: shows the FT-IR spectrum recorded in the range 400-4000 cm⁻¹ to identify the functional groups present in CLE. From FT-IR, It was observed that aromatic molecules with following functional groups, intermolecular hydrogen bonding and O-H stretching (3448.77 cm⁻¹), -C≡N in nitrile (2347.84 cm⁻¹), -C≡C disubstituted alkyne (2099.34 cm⁻¹), -C-H and C=O stretching in aldehyde (1640.73 cm⁻¹), -C=O stretching in ester (1398.92 cm⁻¹), -C-H stretching -C-O-C- (1115.08 cm⁻¹), and -C-H deformation in alkyne (658.02 cm⁻¹) are present in CLE. Further found that CLE inhibits the corrosion of brass specimen with high efficiency due to the presence of N and O in the organic molecules of CLE [22,23].

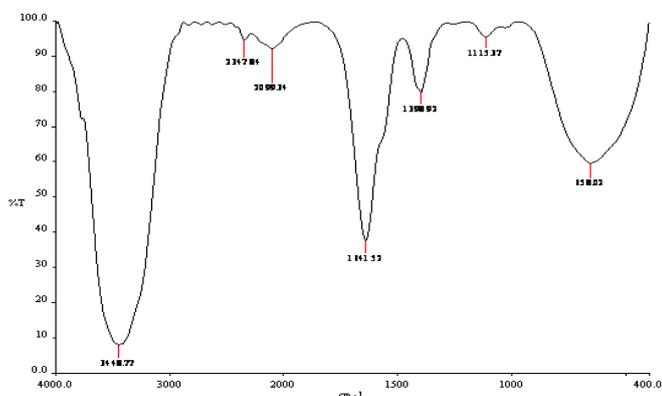
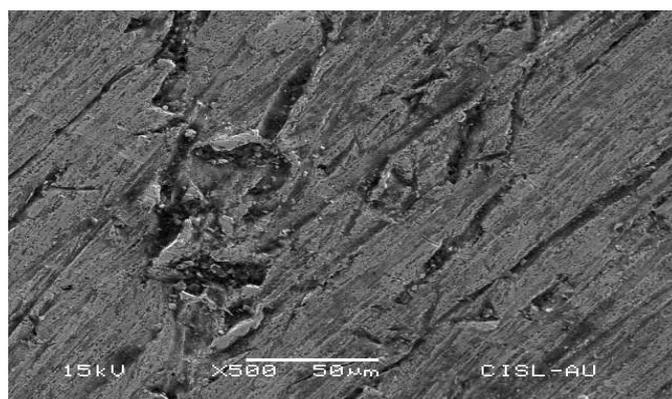


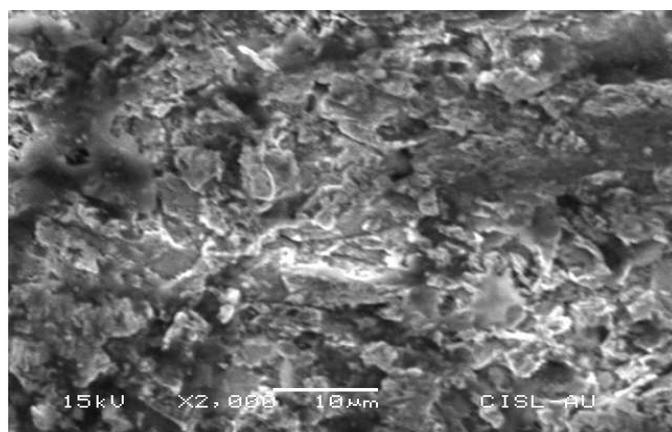
Figure 6: FT-IR spectra of the surface of brass formed by immersing sample in 0.1 N H₃PO₄ with CLE for 6 h

3.5.2 SCANNING ELECTRON MICROSCOPY

SEM micrograms of the polished surface of brass exposed for 6 h in 0.1 N H₃PO₄ in absence and presence of CLE are shown in Figure 7: (a)-(b) shows the surface morphology of brass formed in 0.1 N H₃PO₄ without and with CLE for 6 h. In the comparison of the SEM micrograms, there were a rough surface on brass in absence of extract and a smooth surface with deposited extract in presence of the CLE. This confirms that the extract inhibited corrosion of brass through adsorption of the inhibitor molecules on metal surface. After immersing in the inhibitor containing solution, the entire metal surface was covered with a layer formed with inhibitor as a barrier to corrosion, as denoted by rougher over abrasions. The inhibiting layer was possibly consisting of Cu²⁺ and Zn²⁺ complexes formed with the CLE derivatives are mentioned in FT-IR [24,25].



(a)



(b)

Figure 7: SEM images of brass surface after 6 h immersion in 0.1N H₃PO₄ in the absence (a) and presence (b) of CLE

4. CONCLUSIONS

The inhibition efficiency of CLE on corrosion of brass in 0.1 N H₃PO₄ increases on increasing of concentration of the extract and decreases with rise in temperature. Adsorption of inhibitor molecules of the extract on brass surface is found to obey Tempkin adsorption isotherm. The increase in the values of activation energies of the corrosion process in the presence of extract indicates that CLE creates a physical barrier to charge and mass transfer, leading to reduction in corrosion rate of brass in 0.1 N H₃PO₄. The negative values of ΔG_{ads} and ΔH highlight that the inhibition of corrosion of brass through adsorption is spontaneous and exothermic. Their values

also reveal that physical adsorption is involved in the adsorption process. Potentiodynamic polarization measurements show that CLE acts as a mixed type inhibitor. Inhibition efficiency values were found to show good trend with weight-loss method, potentiodynamic polarization and electrochemical impedance spectroscopy studies. SEM and FT-IR studies confirm that corrosion inhibition of brass in 0.1 N H₃PO₄ is due to adsorption of the CLE extract on brass.

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